# Chapter 18 Use of Receding Horizon Optimal Control to Solve MaxEP-based Biogeochemistry Problems

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Abstract The maximum entropy production (MaxEP) principle has been applied to 7 steady state systems, but biogeochemical problems of interest are typically transient 8 in nature. To apply MaxEP to biogeochemical reaction networks, we propose that 9 living systems maximum entropy production over appropriate time horizons based 10 on strategic information stored in their genomes, which differentiates them from 11 inanimate chemistry, such as fire, that maximizes entropy production instanta-12 neously. We develop a receding horizon optimal control procedure that maximizes 13 internal entropy production over different intervals of time. This procedure involves 14 optimizing the stoichiometry of a reaction network to determine how biological 15 structure is partitioned to reactions over an interval of time. The modeling work is 16 compared to a methanotrophic microcosm experiment that is being conducted to 17 examine how microbial systems integrate entropy production over time when 18 subject to time varying energy input attained by periodically cycling feed-gas 19 composition. The MaxEP-based model agrees well with experimental results, and 20 model analysis shows that increasing the optimization time horizon increases 21 internal entropy production. 22

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## 27 **18.1 Introduction**

In this chapter we examine the application of the maximum entropy production (MaxEP) principle for describing microbial biogeochemistry. Biogeochemistry

enlists the fields of biology and geochemistry to understand chemical transfor-

mations and element cycling that occur in natural environments. Because the

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majority of biologically catalyzed reactions that occur on Earth, such as nitrogen 32 fixation, denitrification, metal redox reactions, sulfate reduction, etc., are orches-33 trated by bacteria and archaea [12], we restrict our current focus to microbially 34 catalyzed reactions. Microbes (including viruses, bacteria and archaea) are the 35 simplest living organisms and are at the interface between chemistry and biology 36 because they catalyzed reactions that also occur abiotically, such as the oxidation 37 of iron (rusting), oxidation of hydrogen sulfide and methane, fixing  $N_2$  into  $NH_3$ 38 and HNO<sub>3</sub> (lightening and combustion). Since we can view bacteria and archaea as 39 simple molecular machines [12], they are most likely amendable to thermody-40 namic description. They are critical for the support and functioning of all higher 41 life on Earth, so it is particularly important to understand how their presence and 42 growth controls the chemistry at local, regional and global scales. Our expectation 43 is that by employing MaxEP we will be able to develop more robust models that 44 can be used to study how biogeochemistry changes as the environment is altered 45 by natural phenomena and human actions. 46

Biogeochemistry can be viewed from two extreme perspectives. In the classic 47 perspective, organisms determine the overall biogeochemical processes that occur 48 in an ecosystem. This organismal centric view derives naturally from reduction-49 ism, as biogeochemistry is by definition a product of organismal growth. However, 50 the organismal centric view implies that changing species composition will likely 51 produce different biogeochemistry. Furthermore, this approach requires detailed 52 knowledge on organism growth kinetics, predator-prey interactions, as well as on 53 how community composition may change as a result of internal dynamics or 54 external drivers. Except for extremely simple systems, this information is usually 55 lacking. Despite these short comings, the majority of biogeochemical models use 56 the organismal perspective as a basis of their design [13]. 57

The second perspective on biogeochemistry takes a systems approach and 58 views ecosystems thermodynamically as open, non-equilibrium systems. In this 59 case, it is free energy potential, resource availability and information that deter-60 mine ecosystem biogeochemistry. While organisms ultimately carry out the pro-61 cess, thermodynamics determines which metabolic functions will dominate. 62 Organisms are viewed as interchangeable components, similar to microstates that 63 underlie macrostates in equilibrium thermodynamics [44]. It is this thermody-64 namic perspective that we will employ to describe ecosystem biogeochemistry, 65 where MaxEP will serve as the governing principle. Because we will limit our 66 analysis to microbial processes, we will remove the typical organismal emphasis 67 and instead view a microbial community in functional terms as a collection of 68 catalysts (or molecular machines [12]) that are synthesized and degraded to 69 achieve MaxEP. 70

In this chapter we develop a MaxEP-based biogeochemical (BGC) model of a distributed metabolic network. Model degrees of freedom are determined by solving a receding horizon optimal control problem that maximizes entropy production over successive intervals of time. Results from the model are compared to data from two methanotrophic microcosm experiments, a control, and a treatment where energy input is cycled over a 20 day period.

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## 77 18.2 MaxEP and Living Systems

The MaxEP conjecture [8, 10, 35, 36] states that steady state, non-equilibrium 78 systems with many degrees of freedom will likely be found in a state that maxi-79 mizes internal entropy production. If internal self-organization, such as vortices 80 and macroscopic structures, facilitates internal entropy production, then those 81 structures will likely develop [26]. Similar to equilibrium thermodynamics that 82 requires systems to be found in the state of maximum entropy, MaxEP indicates 83 that nonequilibrium systems will head towards equilibrium along the fastest 84 possible pathway. That is, they will dissipate free energy as fast as possible within 85 the constraints imposed on the system [28, 44]. As discussed in this book and 86 elsewhere, several phenomena appear consistent with MaxEP, including planetary-87 scale heat transport [19, 27], laminar to turbulent flow transition [29], plant 88 evapotranspiration [46], and many others (see [35] and references therein). 89

## 90 18.2.1 Living Systems as Catalysts

If MaxEP indicates that systems should race down free energy surfaces towards 91 equilibrium as fast as possible, then why isn't the universe already at equilibrium? 92 The answer is because systems often get trapped in metastable states. For instance, 93 a mixture of methane and air at 20 °C, even within the combustible mixture 94 envelope (5–15 %  $CH_4$ ), will remain in this metastable state for a considerable 95 length of time due to the high activation energy required to overcome the repulsive 96 force of the electron cloud that prevents spontaneous reaction. Of course, if a spark 97 is introduce, then the highly exothermic reaction proceeds in a MaxEP manner due 98 to the increase in temperature. Another means in which the free energy can be 99 released is by introducing a catalyst. By reducing the activation energy, the 100 catalyst frees the system from its metastable state, so the reaction can proceed at 101 room temperature even if the system lies outside the combustion envelope or the 102 reactants are dissolved in water. 103

While most man-made catalysis are crude and exhibit poor selectivity, enzyme 104 catalysts synthesized by bacteria, as well as all living organisms, achieve extreme 105 reductions in activation energies along very selective reaction pathways. It is the 106 presence of these enzyme catalysts that hastens the dissipation of free energy and 107 entropy production through the destruction of chemical and electromagnetic 108 potentials. However, the increase in reaction rates provided by catalysts is 109 proportional to the amount of catalyst present. To maximize entropy production, it 110 is necessary for a system to rely on autocatalytic reactions that not only dissipate 111 chemical potential but also synthesize more catalyst in the process, such as the 112 methane oxidation reaction given by, 113

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$$CH_4 + 2O_2 + \Sigma \xrightarrow{\text{(b)}} \mathfrak{S} + H_2CO_3 + H_2O$$
(18.1)

115 116 where  $\mathfrak{S}$  is a catalyst, or *biological structure*, synthesized from available resources, such as C, N, P, Fe, in the environment,  $\Sigma$ . Because catalyst is produced as a 117 product of methane oxidation in Eq. (18.1), the reaction will proceed exponentially 118 provided resources,  $\Sigma$ , needed to build catalyst are not limiting. Of course, 119 Eq. (18.1) also represents growth of methanotrophs (specialized bacteria that eat 120 methane), but we are placing emphasis here on catalyst synthesis for the 121 dissipation of chemical potential, not on the nature of bacterial growth. This 122 distinction represents a paradigm shift from 'we eat food' to 'food has produced us 123 to eat it' [25]. 124

In order to calculate the rate of en action, Eq. (18.1), we need to know the 125 standard molar entropy associated with biological structure, S. Unfortunately, 126 there is considerable confusion associated with entropy calculations involving 127 living organisms. It is often believed that living organisms represent extremely low 128 entropy structures. This misconception can be attributed to confusion over the 129 association between entropy and order. Order, as might be represented by a pat-130 tern, does contribute to entropy, but the entropy (or free energy) of the material the 131 pattern is constructed from must also be accounted for in the entropy calculation. 132 As [34] has shown, only when the pattern is written at the atomic scale does the 133 entropy of the pattern become significant compared to the entropy of the material 134 the pattern is written in. 135

Consider the words written on this page. Because the ink on the page forms a 136 pattern that contains information, the entropy of the page is lower than a page with 137 randomized letters [5]; however, the reduction of entropy is trivial compared to the 138 entropy of the paper the ink is written on. If the paper is burned, it hardly matters 139 in a thermodynamic context if the text contains the meaning of life or only 140 jibberish; the difference in the amount of free energy dissipated, or entropy pro-141 duced, between the two cases is virtually undetectable, because the pattern on this 142 page is written at a macroscopic scale. Likewise, entropy associated with infor-143 mation contained in DNA/RNA or protein is small compared to the entropy 144 associated with the nucleic or amino acid polymers the information is written in 145 [45]. All too often the entropy of the material a pattern is written in is overlooked, 146 which leads to incorrect assessments, such as the popular statement that a clean 147 desk has lower entropy than a messy one; both have the same thermodynamic 148 entropy or free energy. In terms of entropy and free energy calculations, a gram of 149 freeze-dried yeast or bacteria, which are viable upon rehydration, has the same 150 molar entropy and free energy of formation as an equivalent weight of a macro-151 molecules in the appropriate proportions [3]. To paraphrase [34], the *élan vital* 152 carries no thermodynamic burden. 153

While the entropy associated with the information content of a cell is trivial 154 compared to the material of a cell, it is nevertheless of critical importance. It is 155

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useful information [1] contained in the genome that allows for the construction of 156 complex macromolecules that gives rise to the catalytic nature of biological 157 structure, S. Ultimately, then, it is information that releases systems from meta-158 stable states to flow down free energy surfaces and produce entropy. Evolution 159 works to refine this information and thereby increase the rate of entropy produc-160 tion. Information and entropy are intimately coupled [17]. Philosophically, we 161 postulate free energy spawns the creation of information that hastens free energy's 162 destruction. 163

## 164 18.2.2 MaxEP and Transient Systems

An element of time has been implied in the MaxEP description above for con-165 structing biological structure to dissipate free energy; however, all MaxEP theories 166 to date have been applied to steady state systems only, where time is not involved 167 in the equations. There currently does not exist a MaxEP theory for transient 168 systems where the state is allowed to vary with time, but it is transient systems we 169 are often most interested in. The objective in modeling is usually to understand and 170 predict how a system of interest will respond to perturbations or changes in 171 external drivers. To build a transient biogeochemistry model based on MaxEP 172 requires that we speculate as to how time may affect the MaxEP solution. 173

For any particular system we can define internal entropy production once the system boundaries have been defined [32, 35], as well as formulate an entropy balance equation, such as

$$\frac{dS}{dt} = J_S + \dot{\sigma} \tag{18.2}$$

where *S* is system entropy (kJ K<sup>-1</sup>),  $J_S$  is the entropy flux into the system (from mass and heat transport) and  $\dot{\sigma}$  is the entropy production rate due to irreversible processes occurring within the system. The second law requires that  $\dot{\sigma} \ge 0$  [20]. We also define  $\sigma$  as  $\int \dot{\sigma} dt$ , which is the amount entropy that derives from internal irreversible processes over some interval of time. Throughout this manuscript we will only be concerned with  $\sigma$  or  $\dot{\sigma}$ , but not *S*, because MaxEP applies to internal entropy production only.

For a transient system, internal entropy production is a function of time,  $\dot{\sigma}(t)$ , so 186 how can MaxEP be defined when  $\dot{\sigma}$  varies with time? One special case would be to 187 maximize  $\dot{\sigma}$  at every instance in time, which would be equivalent to taking a steepest 188 decent pathway along the free energy surface defined by the current state and all 189 possible pathways leading from that point, similar to water flowing downhill. 190 However, following a steepest decent pathway at each instance in time may not lead 191 to the greatest internal entropy production over an interval of time. Consider 192 Fig. 18.1 for example. Instantaneous internal entropy production at time  $t_n$  is greater 193 along pathway PA than along pathway PB, since  $\dot{\sigma}_A(t_n) > \dot{\sigma}_B(t_n)$ . But taking the 194

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### **Fig. 18.1** Increases in internal entropy over two possible pathways starting from point *P* at time $t_n$ . Here, $\sigma$ is the part of system entropy *S* that is from internal irreversible processes and $\dot{\sigma}$ its production rate



steepest descent pathway at point P sets the system along a trajectory that ultimately 195 produces less internal entropy than had the system followed pathway PB, since 196  $\sigma_B(t_n + \Delta t^*) > \sigma_A(t_n + \Delta t^*)$ . If the system had a means to explore all possible future 197 pathways leading from P over  $\Delta t^*$  time, then the system could increase entropy 198 produced over the steepest descent pathway, PA, by following pathway PB. That is, 199 if the system has a way to generate predictions, then forgoing the steepest descent 200 pathway can lead to greater internal entropy production over time. We postulate that 201 this is precisely what living systems do. 202

Because living systems can store information in their genome, they can develop 203 temporal strategies based on passed events that become refined via evolutionary 204 selection. Genomic information not only allows organisms to access free energy 205 trapped in metastable states, but also allows them to follow pathways that avoid 206 the steepest decent route and produce more entropy over time. For instance, some 207 bacteria form spores or dormant cells that increase their fitness when conditions 208 become hostile [23, 24]. Likewise, many organisms will increase fat storage in the 209 fall to survive the winter months. While temporal strategies are well recognized, 210 they are often not accounted for in models. Instead, most biogeochemistry models 211 view the system as a type of Markov process where system response only depends 212 on the current state. We believe what differentiates abiotic systems from biotic 213 ones, is the ability of the latter to store information that allows them to develop 214 temporal strategies and out compete abiotic systems over time in internal entropy 215 production [44]. Maximizing internal entropy produced over intervals of time is 216 the basis of the model and associated experiment discussed in the next section. 217

# 218 18.3 Methods

Discussed below are descriptions of a microbial microcosm experiment and an associated mathematical model that are intended to explore the idea that living systems develop temporal strategies that increase entropy production when averaged over time. The experimental setup employs methanotrophic microcosms whose energy input is cycled over time, while the modeling of the microcosms is based on a distributed metabolic network of biochemical reactions that are

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controlled to maximize averaged entropy production over intervals of time using a
 receding horizon optimal control approach.

## 227 18.3.1 Experimental System

The experiment is designed to examine how microbial communities adapt and 228 evolve to cope with periodic energy inputs using methane plus air as the sole 229 source of energy. The experimental setup [44] consists of four 18 L microcosms 230 that are operated in chemostat mode at a dilution rate of 0.1  $d^{-1}$  and are sparged at 231 a gas flow rate of 20 mL min<sup>-1</sup> (0 °C, 101.3 kPa). Two control microcosms are 232 sparged continuously with a gas mixture of 4.9 % CH<sub>4</sub>, 19.6 % O<sub>2</sub>, 0.03 % CO<sub>2</sub>, 233 balance N<sub>2</sub>, while two other microcosms are cycled between the methane plus air 234 mixture and just air (20.95 % O<sub>2</sub>, 0.033 % CO<sub>2</sub>, balance N<sub>2</sub>) over a 20 d period 235 (10 days with CH<sub>4</sub> on, 10 days with CH<sub>4</sub> off). All microcosms were inoculated 236 approximately 4 years ago with whole water samples collected from a coastal 237 pond and cedar bog (1 L each). A mineral salts medium (10 mM K<sub>2</sub>HPO<sub>4</sub>, 50 µM 238 KNO<sub>3</sub>, 100 µM MgSO<sub>4</sub>, 100 µM CaCl<sub>2</sub>, 100 µM NaCl, plus trace elements 239 solution) adjusted to pH 6.8 is used as feed. 240

Output gas composition is analyzed on-line every 5 h for CH<sub>4</sub> (NDIR, California 241 Analytical Instruments), O<sub>2</sub> and CO<sub>2</sub> (laser diode adsorption spectroscopy, Oxigraf) 242 concentrations, and analyzer drift is compensated for by monitoring input gas 243 composition. Dissolved oxygen and pH electrodes are measured and recorded every 244 hour. Gas cycling and all data acquisition are under computer control and posted 245 on-line (http://ecosystems.mbl.edu/MEP). Periodically, liquid samples are with-246 drawn for both nutrient analysis (NO<sub>3</sub><sup>-</sup>, NH<sub>3</sub>, particulate organic C (POC), N 247 (PON), dissolved organic C (DOC), and N (DON)) and microbial community 248 assessment via cell counts and 454-tag pyrosequencing of the V4-V6 hypervariable 249 regions of the 16S rRNA gene [16]. 250

## 251 18.3.2 Metabolic Network Model

The MaxEP-based biogeochemistry model uses a distributed metabolic network 252 approach to simulate the functional attributes of a microbial community [43]. For 253 the methanotrophic microcosms, four biological structures are used to capture 254 methane oxidation to methanol  $\mathfrak{S}_1$ , methanol to  $CO_2 \mathfrak{S}_2$ , the turnover of biological 255 structures  $\mathfrak{S}_3$ , and the consumption of recalcitrant (i.e., hard to decompose) 256 organic C (dC) and N (dN),  $\mathfrak{S}_4$  (Table 18.1 and Fig. 18.2). This metabolic network 257 structure differs significantly from our previous approach [44]. Here, we use whole 258 reactions instead of half reactions to represent metabolism, which has two main 259 advantages: (1) since half reactions produce (or consume) electrons, we do not 260 need equations and constraints to insure electron conservation and (2) biological 261

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**Table 18.1** Reaction stoichiometries and optimal control variables (*OCV*:  $\varepsilon_j$  and  $\omega_{i,j}$  in Eq. 18.4) associated with the four biological structures used to represent methanotrophic communities

Reaction		
Rate	Stoichiometry	OCV
<i>r</i> <sub>1,1</sub>	$\mathrm{CH}_{4} + \varepsilon_{1} \gamma_{1} \mathrm{HNO}_{3} + a_{1,1} \mathrm{O}_{2} \xrightarrow{\mathfrak{S}_{1}} \varepsilon_{1} \mathfrak{S}_{1} + (1 - \varepsilon_{1}) \mathrm{CH}_{3} \mathrm{OH} + b_{1,1} \mathrm{H}_{2} \mathrm{O}$	$\mathcal{E}_1, \mathcal{O}_{11}$
<i>r</i> <sub>2,1</sub>	$CH_4 + \varepsilon_1 \gamma_1 NH_3 + a_{2,1}O_2 \xrightarrow{\mathfrak{S}_1} \varepsilon_1 \mathfrak{S}_1 + (1 - \varepsilon_1) CH_3 OH + b_{2,1}H_2 O$	
<i>r</i> <sub>1,2</sub>	$CH_{3}OH + \varepsilon_{2}\gamma_{2}HNO_{3} + a_{1,2}O_{2} \xrightarrow{\circledast_{2}} \varepsilon_{2} \not \gg_{2} + (1 - \varepsilon_{2})H_{2}CO_{3} + b_{1,2}H_{2}O$	$\mathcal{E}_{2}, \mathcal{O}_{12}$
<i>r</i> <sub>2,2</sub>	$CH_{3}OH + \varepsilon_{2}\gamma_{2}NH_{3} + a_{2,2}O_{2} \xrightarrow{\mathfrak{S}_{2}} \varepsilon_{2}\mathfrak{S}_{2} + (1 - \varepsilon_{2})H_{2}CO_{3} + b_{2,2}H_{2}O$	27 1,2
<i>r</i> <sub><i>i</i>,3</sub>	$\begin{split} \boldsymbol{\hat{\varpi}}_{i} + a_{i,3} \mathcal{O}_{2} & \stackrel{\boldsymbol{\hat{\varpi}}_{3}}{\rightarrow} \boldsymbol{\varepsilon}_{3} \boldsymbol{\hat{\varpi}}_{3} \\ &+ (1 - \boldsymbol{\varepsilon}_{3}) [\gamma_{i}(\boldsymbol{\varepsilon}_{3} \mathrm{NH}_{3} + (1 - \boldsymbol{\varepsilon}_{3}) \mathrm{dN}) + \boldsymbol{\varepsilon}_{3} \mathrm{H}_{2} \mathrm{CO}_{3} + (1 - \boldsymbol{\varepsilon}_{3}) \mathrm{dC}] \\ &+ \boldsymbol{\varepsilon}_{3}(\gamma_{i} - \gamma_{3}) \mathrm{NH}_{3} + b_{i,3} \mathrm{H}_{2} \mathrm{O}  \text{for } i = 1, \dots, 4 \end{split}$	$\mathcal{E}_3$
<i>r</i> <sub>1,4</sub>	$dCN + a_{1,4}O_2 \xrightarrow{\mathfrak{B}_4} \varepsilon_4 \mathfrak{B}_4 + (1 - \varepsilon_4)H_2CO_3 + b_{1,4}H_2O + d_{1,4}NH_3$	${\cal E}_4$

Biological structure is unit carbon based and its composition is given by  $CH_{x_j}O_{\beta_j}N_{\gamma_j}$ . The stoichiometric coefficients,  $a_{i,j}$ ,  $b_{i,j}$  and  $d_{1,4}$  are determined from O, H and N elemental balances for each reaction as necessary



structure synthesis is directly coupled to its associated redox reaction pair. Nevertheless, networks based on half reactions are useful for discovering important reaction pairs that evade detection, such as anammox [21], because models based on half reactions build their own redox pair combinations.

Reaction stoichiometries are parameterized by two types of optimal control variables,  $\varepsilon_j$  and  $\omega_{i,j}$ , where the former controls the efficiency of biological structure synthesis, and the latter controls how biological structure is allocated to

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sub-reactions associated with each biological structure (Table 18.1). For instance, 269  $\omega_{1,1}$  determines how  $\mathfrak{B}_1$  is partitioned between nitrate uptake  $(r_{1,1})$  and ammonia 270 uptake  $(r_{2,1})$ . The value of  $\varepsilon_i$  plays a critical role in the model, because as  $\varepsilon_i$ 271 approaches 0 the reaction behaves as pure combustion dissipating substantial 272 amounts of free energy, while as  $\varepsilon_i$  approaches 1 biological structure is synthesized 273 with minimum free energy dissipation and maximum conversation of C substrate 274 into biomass. As discussed above and elsewhere [45], reaction free energy for 275 biological structure synthesis as  $\varepsilon_i$  approaches 1 is still negative or within the 276 neighborhood of 0, but in order to achieve a growth efficiency of near 100 %, 277 reactions must proceed reversibly (i.e., infinitely slowly). This thermodynamic 278 constraint explains why we do not find bacteria opting for an  $\varepsilon_i$  near 1 strategy. 279

The partitioning of labile (i.e., easily degraded) versus detrital C and N in the 280 four reactions associated with biological structure decomposition,  $r_{i,3}$ , is solely 281 determined by  $\varepsilon_3$ . While this is a crude approximation, it has the advantage that no 282 additional parameters are needed. One of the objectives of the model is to limit the 283 number of adjustable parameters and place as many degrees of freedom as possible 284 in the optimal control variables  $\varepsilon_i$  and  $\omega_{i,j}$ . The detrital C (dC) and N (dN) pools 285 are modeled separately, but are treated as a single molecule, dCN, in reaction  $r_{1.4}$ 286 with its concentration,  $c_{dCN}$ , set to  $c_{dC}$  and its N:C ratio given by  $\gamma_{dCN} = c_{dN}/c_{dC}$ . 287

Total internal entropy produced by the microbial community (kJ K<sup>-1</sup>), ignoring small contributions from mixing entropy [45], is readily calculated from the product of reaction rate  $(r_{i,j})$  and the associated reaction free energy  $(\Delta_r G_{r_{i,j}})$ summed over each reaction in the network, as given by,

$$\dot{\sigma}(t) = -\frac{V_L}{T} \sum_{j=1}^{n_{\rm S}} \sum_{i=1}^{n_{\rm Sj}} r_{i,j}(t) \Delta_r G_{r_{i,j}}(t)$$
(18.3)

where  $V_L$  is the liquid volume of the microcosms (m<sup>3</sup>), *T* is temperature (K),  $n_S$  is the number of biological structures (4 in this case), and  $n_{S_j}$  is the number of subreactions associate with  $\mathfrak{S}_j$  (Table 18.1). We use [2] approach for calculating reaction free energies,  $\Delta_r G_{r_{i,j}}$ , that accounts for species concentrations and activity coefficients, and [4] value for the free energy of formation of biological structure (see also [44, 45]).

Reaction rates are given by the following modified Monod kinetics expression [45]

$$r_{i,j} = v_j \varepsilon_j^2 (1 - \varepsilon_j^2) \prod_{k=1}^{n_c} \left( \frac{c_k}{c_k + \kappa_j \varepsilon_j^4} \right)^{\Lambda_{i,j,k}} \omega_{i-1,j} \prod_{l=i}^{n_{\mathrm{S}_j} - 1} (1 - \omega_{l,j}) f_G(\Delta_r G_{r_{i,j}}) c_{\mathrm{S}_j}.$$
 (18.4)

The parameters  $v_j$  and  $\kappa_j$  were chosen to capture bacterial growth kinetics observed in nutrient deplete (i.e., oligotrophic) to nutrient abundant (i.e., eutrophic) conditions. That is,  $v_j$  and  $\kappa_j$  are independent of community composition. The exponent  $\Lambda_{i,j,k}$  is set to either 0 or 1 depending on reaction stoichiometry (Table 18.1) for the  $n_c$  state concentration variables,  $c_k$ , and  $\omega_{l,i}$  determines how

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 $\mathfrak{S}_{j}$  is partitioned to its associated  $n_{S_{j}}$  sub-reactions, where  $\omega_{0,j} = 1$  for all reactions. For all model runs, we assume decomposition of biological structure occurs indiscriminately, so that  $\omega_{i,3} = c_{S_{i+1}} / \sum_{k=1}^{i+1} c_{S_k}$  for  $i = 1, \ldots, 4$ . To insure no reaction proceeds if its free energy of reaction,  $\Delta_r G_{r_{ij}}$ , is greater than zero, the function  $f_G$ is set to,

$$f_G(\Delta_r G_{r_{ij}}) = \begin{cases} 1 - e^{\chi_G \Delta_r G_{r_{ij}}} & \Delta_r G_{r_{ij}} \le 0\\ 0 & \Delta_r G_{r_{ij}} > 0 \end{cases} ;$$
(18.5)

where  $\chi_G$  is chosen for numerical integration criteria, because the  $(1 - \varepsilon_j^2)$  term in Eq. [18.4] imposes an empirical thermodynamic constraint as  $\varepsilon_j$  approaches 1.

Once again, the motivation for Eq. (18.4) is based on minimizing the number of free parameters. Since  $v_j$  and  $\kappa_j$  have predetermined values for all reactions [45], except for reaction  $r_{1,4}$  discussed below, reaction rates solely depend on the values of the optimal control variables and the concentration of the state variables.

A process that is difficult to model is biofilm formation in the MCs. After several hundred days of operation, considerable biomass accumulated on the reactor walls, even though the MCs were gently mixed. While we could have developed a sophisticated biofilm sub-model, this would result in numerous poorly defined additional parameters. Instead, we simply introduce one parameter,  $f_{PL}$ , to represent the fraction of particulate matter (both living and detrital) that is not subject to chemostat washout because it is associated with the biofilm (see Table A.1).

## 330 18.3.3 Optimization Model

To determine how  $\varepsilon_i$  and  $\omega_{i,j}$  must vary over time in order to maximize internal 331 entropy production, we formulate and solve a receding horizon optimal control 332 (RHOC) problem [7, 30]. RHOC is used in many fields. For example, in 333 economics RHOC is used to determine how short-term investments should be 334 allocated to maximize long-term returns, such as in retirement fund management. 335 Because long-term prediction of markets is not perfect, short-term strategies are 336 updated periodically based on current mark conditions. We implement a similar 337 approach and maximize internal entropy production over successive intervals of 338 time as given by, 339 340

$$\max_{(t_{n+1})} \frac{1}{\Delta t^*} \int_{t_n}^{t_n + \Delta t^*} \dot{\sigma}(\tau) e^{-k_w(\tau - t_n)} d\tau \quad where \quad \mathbf{u} = \left[ \boldsymbol{\varepsilon}^T \ \boldsymbol{\omega}^T \right]^T$$
(18.6a)

343 344 **342** 

subject to: 
$$\frac{d\mathbf{x}(t)}{dt} = \mathbf{f}(\mathbf{x}(t), \mathbf{u}(t))$$
 and  $\mathbf{0} < \mathbf{u}(t) \le \mathbf{1}$  (18.6b)

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where  $\Delta t^*$  is the long-term optimization interval from the current time,  $t_n$ , over 346 which entropy production,  $\dot{\sigma}$ , is maximized. A conventional weighting function, 347  $e^{-k_w(t-t_n)}$ . discounts the importance of entropy production as time increases beyond 348  $t_n$  due to uncertainties in predicting future states. After the value of the optimal 349 control variables  $\varepsilon_i$  and  $\omega_{i,i}$ , are determined over the optimization interval 350  $[t_n, t_n + \Delta t^*]$ , the state equations are updated only to  $t_{n+1} = t_n + \Delta t$ , where 351  $\Delta t < \Delta t^*$ , as illustrated in Fig. 18.1. The updating interval,  $\Delta t$ , is typically less than 352  $\Delta t^*$  to minimize discontinuities in state and control variables at the end of an 353 interval. Average internal entropy production over the update interval,  $\Delta t$ , is given 354 by, 355 356

$$\langle \dot{\sigma}(t_{n+1}) \rangle = \frac{1}{\Delta t} \int_{t_n}^{t_n + \Delta t} \dot{\sigma}(\tau) d\tau.$$
(18.7)

Total internal entropy produced over k intervals is given by  $\sigma(t_n : t_{n+k}) = \Delta t \sum_{i=1}^k \langle \dot{\sigma}(t_{n+i}) \rangle$ . Once the state and control variables are updated to  $t_{n+1} = t_n + \Delta t$ , Eq. (18.6a) is used to solve the next optimization interval,  $t_{n+1} + \Delta t^*$  to extend the solution to  $t_{n+2} = t_{n+1} + \Delta t$ ; this iteration is repeated until the desired final simulation time is reached.

The optimization, Eq. (18.6a), is subject to box constraints on the control 364 variables between 0 and 1, and by mass balance constraints on the state variables, 365  $\mathbf{x}(t)$ , given by the differential equations defined by  $\mathbf{f}(\mathbf{x}(t), \mathbf{u}(t))$  in Eq. (18.6b). The 366 state variables for the microcosm experiment consist of nutrient concentrations, 367  $\mathbf{c}(t)$ , gas partial pressures,  $\mathbf{p}(t)$ , and concentration of biological structures,  $\mathbf{c}_{S}(t)$ , so 368 that  $\mathbf{x}(t) = [\mathbf{c}^{T}(t), \mathbf{p}^{T}(t), \mathbf{c}_{S}^{T}(t)]^{T}$ . The mass balance equations are listed in the 369 Appendix (Table A.1). The differential equations were numerically integrated 370 using a high precision method [6] and the optimization problem was solved using a 371 derivative free algorithm (BOBYQA [39]). Control variables are discretized over 372 the  $[t_n, t_n + \Delta t^*]$  interval using  $n_{knots}$  grid points and linear interpolation is used to 373 produce continuous control functions. 374

## 375 **18.4 Results**

Time zero of the microcosm experiments corresponds to 00:00 20 Aug 2010, and on day 210.5 gas cycling of microcosms (MC) 1 and 4 commenced after experimental operating conditions had been finalized, in particular nitrogen-limited growth was achieved. Numerical simulations using the MaxEP-based BGC model were initialized on day 100, which provided sufficient time to achieve steady state conditions prior to gas cycling. Both experimental and modeling results are compared over days 200–500.



**Fig. 18.3** Observed and modeled reactor exit gas concentrations for the controls (MC 2 and 3, *left column*) and cycled (MC 1 and 4, *right column*) microcosms. Modeled predictions are shown as the *orange* (or *grey* in BW) *solid line*, while experimental data are shown as open symbols connected by *dashed lines*. Model results are for  $k_w = 0.230 \text{ d}^{-1}$ ,  $\Delta t = 10 \text{ d}$  and  $\Delta t^* = 20 \text{ d}$ 

Only two model parameters were qualitatively adjusted to achieve reasonable 383 agreement between model results and observations for all four MCs (Figs. 18.3 384 and 18.4). Because detritus is a rather amorphous, non-polymeric material, its 385 decomposition is difficult and is often the rate limiting step in microbial BGC [14]. 386 Consequently, we reduced  $v_4$  in Eq. (18.4) to 35 d<sup>-1</sup> from the standard value of 387 350 d<sup>-1</sup> [45]. We also tuned the biofilm parameter,  $f_{PL}$ , to 0.2. All other parameter 388 values are well-defined constants, such as MC volume, dilution rate, feed 389 concentrations, etc. All model degrees of freedom, other than  $v_4$  and  $f_{PL}$ , reside in 390



Fig. 18.4 Simulated data [orange (or grey) lines] compared to observations of nitrate and ammonium concentrations for the control MCs (MC 2 and 3, left column) and the methane cycled MCs (MC 1 and 4, right column). Also see caption to Fig. 18.3

for different optimal interval parameters values: $k_w$ , $\Delta t$ and $\Delta t^*$						
$\Delta t$	$\Delta t^*$	k <sub>w</sub>	n <sub>knots</sub>	$\sigma(100:500)~({\rm kJ}~{\rm K}^{-1})$		
(d)	(d)	$(d^{-1})$		Control	Cycled	
0.1	0.1	0	1	2.07	1.45	
0.1	1	3.00	5	18.56	7.71	

5

15

20

25

16.82

22.85

24.19

24.64

24.77

6.94

9.05

10.53

14.55

15.15

Table 18.2 Internal entropy produced over 400 days for the control and gas-cycled simulations

the 6 optimal control variables and the three interval optimization parameters,  $k_w$ , 391  $\Delta t$  and  $\Delta t^*$ . 392

To examine how the optimal interval parameters affect the solution and overall 393 internal entropy production, we conducted several simulations by varying  $k_w$ ,  $\Delta t$ 394 and  $\Delta t^*$  for both the control and the gas-cycled simulations (Table 18.2). 395 In general, these results show that as the optimization interval increases, total 396

1

1

10

20

20

1

5

20

40

50

0

0.921

0.230

0.115

0.0921

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internal entropy produced ( $\sigma$ ) over the 400 days of simulation increases, but 397 asymptotes to approximately 25 and 15 kJ K<sup>-1</sup> for the control and gas-cycled 398 simulations, respectively. Except for very short intervals, entropy production in the 399 control simulations is not strongly affected by choices of  $\Delta t$  or  $\Delta t^*$  (Table 18.2). 400 However, for very short optimization intervals ( $\Delta t^* = 0.1$  d), entropy production is 401 significantly depressed (Table 18.2). A similar phenomenon occurs in the gas-402 cycled simulations, but the decrease in total entropy production as  $\Delta t^*$  decreases is 403 more gradual. 404

As  $\Delta t^*$  becomes small, biological structures are allocated to maximize entropy 405 production in a manner that resembles abiotic systems, such as fire. In particular, 406 examination of the control simulations reveals that the system does not sufficiently 407 allocate resources to biological structure turnover,  $\mathfrak{S}_3$ . The concentration of  $\mathfrak{S}_3$  in 408 the control simulation with  $\Delta t^* = 0.1$  is approximately equal to  $\mathfrak{B}_1$  and  $\mathfrak{B}_2$ , but in 409 the simulation with larger  $\Delta t^*$  values,  $\mathfrak{S}_3$  concentration is twice that of  $\mathfrak{S}_1$  and  $\mathfrak{S}_2$ . 410 The optimal controller attains higher concentration of  $\mathfrak{S}_3$  by setting  $\varepsilon_3$  to 411 approximately 0.62, while in the low entropy producing case  $\varepsilon_3$  is only set to 0.34. 412 The higher concentration of  $\mathfrak{B}_3$  allows the system to achieve much higher 413 remineralization rates, so that reactions  $r_{2,1}$  and  $r_{2,2}$  can attain much higher rates 414 due to the increase in NH<sub>3</sub> availability from S; turnover. However, under short 415 optimization intervals, the system's time horizon is too short to realize a return on 416 investment in \$\mathbf{S}\_3\$ with respect to entropy production or utilization of available 417 chemical potential. When the time scale is short, the system does not make best 418 use of available resources. 419

The gas-cycled simulations also generate interesting results when different 420  $(\Delta t, \Delta t^*)$  values are examined. Figure 18.5a shows methanol dynamics over two 421 gas cycling periods (40 d, beginning on day 300) for four selected simulations in 422 Table 18.2 based on the  $(\Delta t, \Delta t^*)$  values. When time scales are short, 423  $(\Delta t, \Delta t^*) = (0.1, 1 \text{ d})$  and (1, 5 d), methanol (CH<sub>3</sub>OH) accumulates immediately 424 after methane gas is turned on (at 300.5 and 320.5 d; Fig. 18.5a, dashed lines). 425 However, when the time scale specified by the optimization parameters approach 426 the period length of the gas cycling,  $(\Delta t, \Delta t^*) = (10, 20 \text{ d})$  and (20, 50 d), 427 methanol accumulation occurs immediately before methane is switched off (at 428 310.5 and 330.5 days; Fig. 18.5a, solid lines). When the optimization time scales 429 are long, the model develops an anticipatory control strategy, where methanol is 430 produced as a storage compound that can be utilized during the phase when 431 methane is absent. By storing some of the methane captured in the first half of the 432 cycle as methanol, the system is able to oxidize more methane and produce more 433 internal entropy compared to the simulations using short term optimization 434 parameters. The strategy only accumulates methanol near the end of the period, 435 because methanol is also lost due to dilution, which does not contribute to internal 436 entropy production. 437

We can see how the control strategy achieves methanol accumulation by examining the concentration of biological structures and growth efficiencies for the case where  $(\Delta t, \Delta t^*)$  equals (20, 50 d) over the two gas cycling periods

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Fig. 18.5 (a) Methanol accumulation over two cycles for the optimization intervals given in the legend:  $(\Delta t, \Delta t^*)$ . The bar along the x axis shows when CH<sub>4</sub> gas is on (*black*) and off (*white*). Biological structures (**b**) and growth efficiencies (**c**) over two cycle periods for  $(\Delta t, \Delta t^*) = (20 \text{ d}, 50 \text{ d})$ . All data are from the gas-cycled simulations only



(Fig. 18.5b, c). Just prior to the loss of methane (310.5 and 330.5 d), there is an 441 increase in  $\mathfrak{S}_1$  and a decrease in  $\mathfrak{S}_2$  (Fig. 18.5b). Based on the reaction network 442 (Fig. 18.2, Table 18.1), this allocation of catalyst favors methanol overproduction, 443 so methanol accumulates rapidly. Immediately following the addition of methane, 444 there is a rapid rise in  $\mathfrak{S}_2$  concentration and a decrease in  $\mathfrak{S}_1$ , which drives 445 methanol consumption up. To attain these changes in  $\mathfrak{S}_1$  and  $\mathfrak{S}_2$  abundances, there 446 are the expected changes in the associated growth efficiencies (Fig. 18.5c), but 447 there is also a large change in  $\varepsilon_3$ . In particular,  $\varepsilon_3$  is driven to 1 following the loss 448 of methane feed, which allows all biological structures to remain at high 449 concentrations in the absence of methane because  $r_{i,3}$  is driven to zero (Eq. 18.4). 450 Just prior to the introduction of methane,  $\varepsilon_3$  is reduced significantly, which causes 451

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a large turnover of biological structure (Fig. 18.5b), but biological structure
concentrations quickly rebound once methane is again made available. To examine
if these changes are occurring in the actual microcosms, we are currently sampling
for cell abundances, DNA/RNA, and methanol concentration.

## 456 18.5 Discussion

In this chapter we have shown that a microbial biogeochemistry model based on 457 the MaxEP principle produces results that are comparable to those obtained 458 experimentally from microbial methanotrophic microcosms (Figs. 18.3 and 18.4). 459 Unlike most microbial biogeochemistry models, the MaxEP model contains very 460 few adjustable parameters, because we have been able to place most of the model's 461 degrees of freedom into the optimal control variables,  $\varepsilon_i$  and  $\omega_{i,i}$ , whose values are 462 determined by maximizing internal entropy production. By placing emphasis on 463 catalytic activity at the system level, rather than on competition of individuals, the 464 MaxEP approach provides a unique perspective on how ecosystems may function 465 and evolve. Due to the novelty of the MaxEP approach, many of the ideas and 466 conjectures that derive from MaxEP need to be tested, or at least shown to be 467 improvements over canonical approaches. Microbial microcosms provide excel-468 lent experimental systems for testing MaxEP-based approaches for describing 469 living systems, as microbial systems have fast characteristic times scales, high 470 population densities and high biodiversity, all of which can be readily manipulated 471 and monitored. 472

The MaxEP-BGC model predicts a comprehensive suite of output variables that 473 can be compared to observations, only some of which were presented here. In 474 addition to providing concentration data and reaction efficiencies, the model 475 predicts reaction rates through the metabolic network (Table 18.1), reaction free 476 energies, and how biological structure partitioning among sub-reactions changes 477 over time (i.e.,  $\omega_{i,i}$ ). We expect our on-going measurements of community 478 composition from 454-tag pyrosequencing and quantitative PCR analysis of 479 function gene levels and expression will assist in comparing model output to 480 observations [15]. Preliminary molecular results show that very high microbial 481 diversity is maintained in the microcosms ( $\sim 600$  operational taxonomic units); 482 however, community composition of the methanotrophs changes substantially over 483 time (microscopic behavior), but this does not alter methane oxidation rates 484 (macroscopic behavior), a characteristic consistent with MaxEP [9]. 485

Perhaps the most intriguing result from our implementation of MaxEP for describing microbial biogeochemistry is the proposed distinction between abiotic and biotic systems based on instantaneous versus averaged entropy production. When entropy production is maximized instantaneously, no biological structure is produced because some of the free energy would simply be converted to another form of chemical potential instead of being destroyed. This problem is solved by

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maximizing entropy produced over an interval of time, which leads to the 492 hypothesis. Because biotic systems are able to store information in their genome. 493 they can implement temporal strategies that can out-compete abiotic processes in 494 some situations. Because of genomic complexities, we do not know a priori the 495 nature of the temporal strategies at this time, but this lack of knowledge can 496 be circumvented by assuming that evolution has produced systems that extract the 497 greatest possible free energy from a system over some appropriate characteristic 498 time scale. Our results indicate (Table 18.2) that the longer the time scale, the 499 more entropy that can be produced, but longer time scales require higher fidelity in 500 predicting future states. Prediction in this case simply means that some of the 501 temporal strategies the system possesses will be successful. Mismatches between 502 prediction and the true state, due to perturbations, noise and uncertainties, 503 ultimately limit the time scale interval for entropy production. 504

Our receding horizon optimal control implementation of the MaxEP problem 505 shows that when time scales are short, biological structure should be invested for 506 immediate entropy production, which leads to methanol production following the 507 introduction of methane (Fig. 18.5a, dashed lines). This is an R-selection strategy 508 [38], which is a possible driving mechanism for cross feeding [40], because partial 509 substrate oxidation can increase growth rate [37]. When time scale is increased, 510 the system allocates resources to  $\mathfrak{B}_3$  (the equivalent of grazers) as well as the later 511 production of methanol that acts as a storage compound (Fig. 18.5a, solid lines). 512 Systems oriented analyses of natural ecosystems indicate that the presence of 513 grazers increases nutrient recycling and ecosystem productivity [31, 41, 42]. 514 Predators, and trophic structures in general, increase the characteristic time scale 515 of an ecosystem. It appears reasonable that organisms with long development 516 times, or life histories, impart the long characteristic time scales observed in 517 mature ecosystems, such as forests. Under this conjecture, bacterial systems may 518 be closer to fire than an ecosystem composed of macroscopic organisms that 519 provide the long characteristic time scale with respect to entropy production. 520

Experimentally, we expected more effective use of  $CH_4$  in the gas-cycled 521 treatment; that is, we expected entropy production to be similar between the 522 control and gas-cycled MCs. Interestingly, the MaxEP-BGC model also has 523 difficulties in producing entropy in the gas-cycled MCs (Table 18.2), but matches 524 the experimental data well (Figs. 18.3 and 18.4). Because of methanol washout 525 from the chemostat, the model only uses methanol as a storage compound near the 526 end of the CH<sub>4</sub>-on cycle, which limits the system's ability to store chemical 527 potential. Storage of free energy in biological structure is also limited due to N 528 requirements for S. Perhaps the experiment and model are lacking higher trophic 529 levels (i.e., macrofauna) that would provide a time scale relevant to the 20 day 530 gas-cycle period. Currently, the model uses cannibalism of  $\mathfrak{B}_3$  as a means of 531 trophic closure [33], so adding additional trophic levels may be one means 532 of increasing the characteristic time scale in the model. As for the experiment, we 533 are currently characterizing the eukaryotic community structure via cell counts. 534

<sup>535</sup> Our MaxEP-BGC model currently focuses on microbes as reaction catalysts that <sup>536</sup> dissipate chemical potential, but the MaxEP concept can be extended to macro-

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fauna and-flora as well. Metabolically, macroorganisms are rather prosaic; however, in addition to their longer characteristic time scales, they provide physical structure, increase the surface area of particulate matter via mastication and greatly enhance transport processes that often limit reaction rates [11, 18, 22]. Application of MaxEP to natural ecosystems will require understanding the functional contributions of macroorganisms, in particular with respect to transport processes, which is not a typical focus in ecology. More research needs to be done in this area.

## 544 **18.6 Conclusions**

We have been able to use the MaxEP conjecture to develop a microbial biogeo-545 chemistry model that reproduces reasonably well experimental data obtained from 546 a methanotrophic microcosm experiment. By assuming that genomic information 547 allows living systems to maximize entropy production over a characteristic time 548 scale, we have been able to formulate the model as a receding horizon optimal 549 control problem. Most of the model's degrees of freedom have been captured by 550 the optimal control variables whose values are determined by maximizing entropy 551 production over successive intervals of time. This approach greatly reduces the 552 number of adjustable parameters whose values are often unknown, poorly con-553 strained and seldom constant. Our results indicate that temporal strategies that are 554 successful over greater durations of time will result in greater entropy production. 555 From this hypothesis, we have developed a methanotrophic microcosm experiment 556 to study how microbial communities respond, adapt and evolve to time varying 557 inputs of energy. Based on experimental data to date, there appears to be good 558 agreement between the MaxEP-BGC model results and experimental data. 559

All organisms possess genomic and acquired information that dictates survival 560 strategies and life cycles that operate over defined characteristic time scales. These 561 time scales can be as short as minutes or hours (i.e., for some bacteria) to as long 562 as centuries or more (i.e., some tree species). Our approach has illustrated the 563 importance that temporal strategies have on ecosystem dynamics, but our choice of 564 time scale (for both  $\Delta t$  and  $\Delta t^*$ ) has been somewhat arbitrary based on our intuitive 565 understanding of bacterial growth and the reduced complexity of our experimental 566 microcosms. Natural ecosystems are comprised of populations of different 567 organisms that operate over a multitude of time scales. However, we hypothesize 568 that organisms with long time scales can access more free energy (and ultimately 569 producing more entropy) than those operating on short time scales provided the 570 system is stable enough for long term predictions. Viewing ecosystems as a 571 collection of free energy dissipating machines adaptively operating over a spec-572 trum of time scales may help us understand how these systems assemble, operate 573 and respond to disturbances of differing magnitude and frequency. Further 574 research is needed relating the ecological concepts of temporal strategies and 575 succession to quantitative measures and representations of time scales for the 576 dissipation of free energy. 577

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#### Appendix 582

Tables A.1 and A.2. 583



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Table A.1 Mass balance equations for the rates of change of chemical species concentrations in the microcosm model used for constraints in Eq. (18.6b)\*

$$\begin{split} \dot{c}_{\mathrm{CH}_4}(t) &= -r_{1,1} - r_{2,1} + \left(F_L(c_{\mathrm{CH}_4}^I - c_{\mathrm{CH}_4}) + k_L a(p_{\mathrm{CH}_4}/k_{\mathrm{CH}_4}(T) - c_{\mathrm{CH}_4})\right)/V_L \\ \dot{c}_{\mathrm{CH}_3\mathrm{OH}}(t) &= (1 - \varepsilon_1)(r_{1,1} + r_{2,1}) - r_{1,2} - r_{2,2} \\ &+ \left(F_L(c_{\mathrm{CH}_3\mathrm{OH}}^f - c_{\mathrm{CH}_3\mathrm{OH}}) + k_L a(p_{\mathrm{CH}_3\mathrm{OH}}/k_{\mathrm{CH}_3\mathrm{OH}}(T) - c_{\mathrm{CH}_3\mathrm{OH}})\right)/V_L \\ \dot{c}_{\mathrm{H}_2\mathrm{CO}_3}(t) &= (1 - \varepsilon_2)(r_{1,2} + r_{2,2}) + \varepsilon_3(1 - \varepsilon_3) \sum_{i=1}^4 r_{i,3} + (1 - \varepsilon_4)r_{1,4} \\ &+ \left(F_L(c_{\mathrm{H}_2\mathrm{CO}_3}^f - c_{\mathrm{H}_2\mathrm{CO}_3}) + k_L a(p_{\mathrm{CO}_2}/k_{\mathrm{H}_2\mathrm{CO}_3}(T) - c_{\mathrm{H}_2\mathrm{CO}_3})\right)/V_L \\ \dot{c}_{dC}(t) &= (1 - \varepsilon_3)^2 \sum_{i=1}^4 r_{i,3} - r_{1,4} + F_L(c_{dC}^f - f_{PL}c_{dC})/V_L \\ \dot{c}_{\mathrm{HNO}_3}(t) &= -\varepsilon_1\gamma_1r_{1,1} - \varepsilon_2\gamma_2r_{2,2} + \varepsilon_3 \sum_{i=1}^4 ((2 - \varepsilon_3)\gamma_i - \gamma_3)r_{i,3} + d_{1,4}r_{1,4} + F_L(c_{\mathrm{NH}_3}^f - c_{\mathrm{NH}_3})/V_L \\ \dot{c}_{\mathrm{NH}_3}(t) &= -\varepsilon_1\gamma_1r_{2,1} - \varepsilon_2\gamma_2r_{2,2} + \varepsilon_3 \sum_{i=1}^4 ((2 - \varepsilon_3)\gamma_i - \gamma_3)r_{i,3} + d_{1,4}r_{1,4} + F_L(c_{\mathrm{NH}_3}^f - c_{\mathrm{NH}_3})/V_L \\ \dot{c}_{\mathrm{O}_2}(t) &= (1 - \varepsilon_3)^2 \sum_{i=1}^2 a_{i,i}r_{i,3} - \gamma_{dCN}r_{1,4} + F_L(c_{dN}^f - f_{PL}c_{dN})/V_L \\ \dot{c}_{\mathrm{O}_2}(t) &= (-\sum_{i=1}^2 \sum_{j=1}^2 a_{i,j}r_{i,j} - \sum_{i=1}^4 a_{i,3}r_{i,3} - a_{1,4}r_{1,4} + \left(F_L(c_{\mathrm{O}_2^f - c_{\mathrm{O}_2}) + k_La(p_{\mathrm{O}_2/k_{\mathrm{O}_2}(T) - c_{\mathrm{O}_2})\right)/V_L \\ \dot{p}_{\mathrm{CH}_4}(t) &= \left(F_G(p_{\mathrm{CH}_4}^f - p_{\mathrm{CH}_4}) + k_LaRT(c_{\mathrm{CH}_4} - p_{\mathrm{CH}_4/k_{\mathrm{CH}_4}(T))\right)/V_G \\ \dot{p}_{\mathrm{CO}_2}(t) &= \left(F_G(p_{\mathrm{CH}_4}^f - p_{\mathrm{CH}_4}) + k_LaRT(c_{\mathrm{CH}_4} - p_{\mathrm{CH}_4/k_{\mathrm{CH}_3}\mathrm{OH}/\mathrm{CH}_3\mathrm{OH}(T))\right)/V_G \\ \dot{p}_{\mathrm{O}_2}(t) &= \left(F_G(p_{\mathrm{O}_2}^f - p_{\mathrm{O}_2}) + k_LaRT(c_{\mathrm{O}_2} - p_{\mathrm{O}_2/k_{\mathrm{O}_2}}(T))\right)/V_G \\ \dot{p}_{\mathrm{O}_2}(t) &= \left(F_G(p_{\mathrm{O}_2}^f - p_{\mathrm{O}_2}) + k_LaRT(c_{\mathrm{O}_2} - p_{\mathrm{O}_2/k_{\mathrm{O}_2}}(T))\right)/V_G \\ \dot{p}_{\mathrm{O}_2}(t) &= \left(F_G(p_{\mathrm{O}_2}^f - p_{\mathrm{O}_2}) + k_LaRT(c_{\mathrm{O}_2} - p_{\mathrm{O}_2/k_{\mathrm{O}_2}}(T))\right)/V_G \\ \dot{c}_{\mathrm{S}_j}(t) &= \varepsilon_j \sum_{i=1}^{n_{ij}} r_{ij} - r_{ij}^3 + F_L(c_{\mathrm{S}_j}^f - f_{PL}c_{\mathrm{S}_j})/V_L \quad \text{for } j = 1, \dots, 4$$

\*The superscript f refers to concentration of variables in the feed stream,  $F_L$  and  $F_G$  are the liquid and gas volumetric feed rates, respectively,  $k_L a$  is the liquid-side mass transfer coefficient,  $k_h(T)$ is a Henry's law coefficient for solute h,  $V_G$  is the gas headspace volume, and  $f_{PL}$  is the fraction of particulate matter loss due to dilution; that is, not associated with the biofilm

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Table A.2	Nomenclature
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VariableDefinitionUnits $a_{i,j}$ Oxygen stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $b_{i,j}$ Water stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $b_{i,j}$ Water stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $mmol m^{-3}$ $c_i^{i}$ Concentration of species $i$ in microcosm feed $mmol m^{-3}$ $c_j^{i}$ Concentration of biological structure $j$ $mmol m^{-3}$ $d_{i,j}$ Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $mmol m^{-3}$ $d_i$ Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $mmol m^{-3}$ $d_i$ Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1) $mmol m^{-3}$ $d_i$ Ammonia stoichiometric coefficient, liquid side $m^3 d^{-1}$ $k_i$ Optimization discounting parameter $m^3 d^{-1}$ $n_i$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $mmol m^{-3} d^{-1}$ $n_i$ Number of sub-reactions associated with $\mathbf{D}_j$ $p_i$ $Pa$ $p_i$ Partial pressure of gas species $i$ $Pa$ $p_i^{f}$ Partial pressure of gas species $i$ $Pa$ $r_i$ Reaction rate $mmol m^{-3} d^{-1}$ $\Delta t$ Optimization interval $d$ $\Delta t$ Optimization interval $d$ $\Lambda^r$ Time $d$ $mol m^{-3} d^{-1}$ $d$ $mol m^{-3} d^{-1}$ $d$ $f_i$ Eaction rate $mmol m^{-3} d^{-1}$	Table A.		
$a_{ij}$ Oxygen stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1) $b_{ij}$ Water stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1) $c_i$ Concentration of species $i$ (c in vector form) $c_i^{\prime}$ Concentration of species $i$ in microcosm feed $c_{ij}$ Anmonia stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1)dcDetrital organic carbondNDetrital organic carbonfr_LFraction of particulate matter loss due to dilutionfVector function of state equations (see Table A1) $k_{La}$ Air-water gas transfer coefficient, liquid side $k_{w}$ Optimization discounting parameter $n_{c}$ Number of chemical species $n_{max}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_{s}$ Number of sub-reactions associated with $\widehat{\mathfrak{S}}_{j}$ $p_{i}$ Partial pressure of gas species $i$ $p_{i}$ Pattial pressure of gas species $i$ $p_{i}$ Quimization interval $d$ d $d$ d $d$	Variable	Definition	Units
$      b_{ij} \qquad \text{Water stoichiometric coefficient for reaction } r_{i,j} (\text{see Table 18.1}) \qquad \text{mmof } \mathbf{m}^{-3} \\ c_i \qquad \text{Concentration of species } i (\mathbf{c} in vector form) \qquad \text{mmof } \mathbf{m}^{-3} \\ c_i \qquad \text{Concentration of species } i (\mathbf{c} in vector form) \qquad \text{mmof } \mathbf{m}^{-3} \\ c_i \qquad \text{Concentration of species } i (\mathbf{c} in vector form) \qquad \text{mmof } \mathbf{m}^{-3} \\ c_i \qquad \text{Concentration of biological structure } j \qquad \text{mmof } \mathbf{m}^{-3} \\ d_i \qquad \text{Annmonia stoichiometric coefficient for reaction } r_{i,j} (\text{see Table 18.1}) \\ dC \qquad \text{Detrital organic carbon} \\ dN \qquad \text{Detrital organic nitrogen} \\ f_{r} \qquad \text{Fraction of particulate matter loss due to dilution} \\ f \qquad \text{Vector function of state equations (see Table A1)} \\ k_i(T) \qquad \text{Henry's law coefficient for solute } i \\ k_ia \qquad \text{Air-water gas transfer coefficient, liquid side} \\ k_w \qquad \text{Optimization itscounting parameter} \\ n_k \qquad \text{Number of chemical species} \\ n_{knots} \qquad \text{Number of sub-reactions associated with } \mathbf{\hat{\$}_j} \\ p_i \qquad \text{Partial pressure of gas species } i \\ p_i \qquad \text{Partial pressure of gas species } i \\ p_i \qquad \text{Partial pressure of gas species } i \\ not \qquad \text{Optimization interval} \\ d \\ d \\ t \qquad \text{Time} \qquad d \\ \mathbf{u} \qquad \text{Vector of control variables } (c, \boldsymbol{\omega}) \\ \mathbf{x} \qquad \text{Vector of control variables } (c, \boldsymbol{\omega}) \\ \mathbf{x} \qquad \text{Vector of state variables } (c, \boldsymbol{\mu}, \mathbf{e}_s) \\ F_G \qquad \text{Gas constant (units depend on equation)} \\ S \qquad \text{System entropy} \qquad \text{kJ K}^{-1} \\ \mathbf{\hat{\$}_j \qquad \text{Biological structure } j \\ \text{tatual units atom formula for biological structure } i \\ P_G \qquad \text{Gas volume of microcosms} \qquad \mathbf{m}^{-3} \\ \mathbf{mond } \mathbf{m}^{-3} \\ T \qquad \text{Temperature} \qquad K \\ V_G \qquad \text{Gas volume of microcosm} \\ a_i \qquad \text{Hydrogen atoms in unit carbon formula for biological structure } i \\ \beta_i \qquad \text{Oxygen atoms in unit carbon formula for biological structure } i \\ \beta_i \qquad \text{Oxygen atoms in unit carbon formula for biological structure } i \\ \beta_i \qquad \text{Oxygen atoms in unit carbon formula for biological structure } i \\ \beta_i \qquad \text{Substrate affinity parameter in reaction } r_{i,j} \qquad \text{Tmod } \mathbf{m}^{-3} \\ mm$	$a_{i,j}$	Oxygen stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1)	
$c_i$ Concentration of species $i$ (c in vector form)mmol m <sup>-3</sup> $c_i^f$ Concentration of species $i$ in microcosm feedmmol m <sup>-3</sup> $c_s$ Concentration of biological structure $j$ mmol m <sup>-3</sup> $d_{ij}$ Ammonia stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1)mmol m <sup>-3</sup> dCDetrital organic carbonfr.Fraction of particulate matter loss due to dilutionfVector function of state equations (see Table A1)ft. $k_i(T)$ Henry's law coefficient for solute $i$ Pa m <sup>3</sup> mmol <sup>-1</sup> $k_a$ Air-water gas transfer coefficient, liquid sidem <sup>3</sup> d <sup>-1</sup> $k_w$ Optimization discounting parameterd <sup>-1</sup> $n_c$ Number of chemical speciesn $n_{mots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of biological structures, $\widehat{\gg}_j$ $n_i$ Partial pressure of gas species $i$ in feed gas $p_i^f$ Partial pressure of gas species $i$ in feed gas $r_i$ Reaction rate $\Delta t$ Optimization interval <t< td=""><td><math>b_{i,j}</math></td><td>Water stoichiometric coefficient for reaction <math>r_{ij}</math> (see Table 18.1)</td><td></td></t<>	$b_{i,j}$	Water stoichiometric coefficient for reaction $r_{ij}$ (see Table 18.1)	
$c_{i}^{f}$ Concentration of species $i$ in microcosm feedmmol m <sup>-3</sup> $c_{S_{j}}$ Concentration of biological structure $j$ mmol m <sup>-3</sup> $d_{i,j}$ Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1)mmol m <sup>-3</sup> $dC$ Detrital organic carbonf $dN$ Detrital organic nitrogen $f_{PL}$ Fraction of particulate matter loss due to dilutionf $k_i(T)$ Henry's law coefficient for solute $i$ $k_{La}$ Air-water gas transfer coefficient, liquid sidem <sup>3</sup> d <sup>-1</sup> $k_{k}$ Optimization discounting parameterd <sup>-1</sup> $n_c$ Number of chemical speciesn $n_{knos}$ Number of gid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of sub-reactions associated with $\mathfrak{S}_{j}$ $p_i$ Partial pressure of gas species $i$ in feed gasPa $r_{ij}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t$ Optimization intervald $\Delta t$ Optimization intervald $\Delta t$ Optimization intervald $\Delta t$ Optimization intervalf $\Lambda t$ Timed $T$ Timef <td>Ci</td> <td>Concentration of species <math>i</math> (c in vector form)</td> <td><math>mmol m^{-3}</math></td>	Ci	Concentration of species $i$ (c in vector form)	$mmol m^{-3}$
$c_{S_j}$ Concentration of biological structure $j$ mmod $m^{-3}$ $d_{i,j}$ Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1)dCdCDetrital organic carbonfrdNDetrital organic nitrogen $f_{rL}$ Fraction of particulate matter loss due to dilutionfVector function of state equations (see Table A1) $k_l a$ Air-water gas transfer coefficient, liquid side $k_w$ Optimization discounting parameter $n_c$ Number of chemical species $n_{kmots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of sub-reactions associated with $\widehat{\Rightarrow}_j$ $p_i$ Partial pressure of gas species $i$ $p_i$ Partial pressure of gas species $i$ in feed gas $r_{ij}$ Reaction rate $M^*$ Optimization interval $d$ $d$ $d$ $d$ $d$ $d$ $d_i$ Vector of control variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ ) $\mathbf{x}$ Vector of state variables ( $c, \boldsymbol{\omega}$ )	$c_i^f$	Concentration of species i in microcosm feed	mmol m <sup>-3</sup>
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	$c_{\mathbf{S}_j}$	Concentration of biological structure j	mmol m <sup>-3</sup>
dCDetrital organic carbondNDetrital organic nitrogen $f_{rL}$ Fraction of particulate matter loss due to dilutionfVector function of state equations (see Table A1) $k_La$ Air-water gas transfer coefficient, liquid side $k_La$ Air-water gas transfer coefficient, liquid side $k_w$ Optimization discounting parameter $n_c$ Number of chemical species $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of biological structures, $\widehat{\mathfrak{S}}_j$ $n_s$ Number of sub-reactions associated with $\widehat{\mathfrak{S}}_j$ $p_i$ Partial pressure of gas species $i$ $p_i$ Partial pressure of gas species $i$ in feed gas $r_{ij}$ Reaction rate $\Delta t$ Optimization update interval $\Delta t$ Optimization interval $d$ $d$ $t$ Time <t< td=""><td><math>d_{i,j}</math></td><td>Ammonia stoichiometric coefficient for reaction <math>r_{i,j}</math> (see Table 18.1)</td><td></td></t<>	$d_{i,j}$	Ammonia stoichiometric coefficient for reaction $r_{i,j}$ (see Table 18.1)	
dNDetrital organic nitrogen $f_{PL}$ Fraction of particulate matter loss due to dilution $f$ Vector function of state equations (see Table A1) $k_i(T)$ Henry's law coefficient for solute $i$ $k_{ka}$ Air-water gas transfer coefficient, liquid side $k_{w}$ Optimization discounting parameter $n_c$ Number of chemical species $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of sub-reactions associated with $\widehat{\gg}_j$ $p_i$ Partial pressure of gas species $i$ $p_i$ Partial pressure of gas species $i$ in feed gas $r_{ij}$ Reaction rate $mol m^{-3} d^{-1}$ $\Delta t$ Optimization update interval $\Delta t$ Optimization interval $d$ $\Delta t^*$ Optimization interval $t$ Time $u$ Vector of control variables ( $e, o$ ) $\mathbf{x}$ Vector of state variables ( $e, \mathbf{p}, \mathbf{e}_s$ ) $F_G$ Gas flow rate to microcosms $\Delta_r G_{r_{ij}}$ Gibbs free energy of reaction $r_{ij}$ $R$ Gas constant (units depend on equation) $S$ System entropy $k$ $K^{-1}$ $\hat{\mathcal{S}_j}$ Biological structure $j$ that catalyzes reaction $r_{ij}$ $T$ Temperature $K$ $K_G$ $Gas volume of microcosma_iHydrogen atoms in unit carbon formula for biological structure i\beta_iOxygen atoms in unit carbon formula for biological structure i\beta_i$	dC	Detrital organic carbon	
$f_{\rm FL}$ Fraction of particulate matter loss due to dilution $f$ Vector function of state equations (see Table A1) $k_i(T)$ Henry's law coefficient for solute i $k_La$ Air-water gas transfer coefficient, liquid side $k_ka$ Air-water gas transfer coefficient, liquid side $n_c$ Number of chemical species $n_{cc}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of sub-reactions associated with $\widehat{\mathfrak{S}}_j$ $n_s$ Number of gas species i $p_i$ Partial pressure of gas species i in feed gas $p_i$ Partial pressure of gas species i in feed gas $r_{ij}$ Reaction rate $Time$ d $d$ U $\Delta t$ Optimization interval $d$ d $d$ $d$ $t$ Time $u$ Vector of control variables ( $\mathfrak{e}, \mathfrak{w}$ ) $\mathbf{x}$ Vector of state variables ( $\mathfrak{e}, \mathfrak{p}, \mathfrak{e}_3$ ) $F_L$ Liquid flow rate to microcosms $M^3 d^{-1}$ $R$ Gas constant (units depend on equation) $S$ System entropy $\mathcal{S}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $T$ Temperature $V_G$ Gas volume of microcosm $\mathfrak{a}_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\beta_i$ Growth efficiency for biological structure $i$ $r_i$ Substrate affinity parameter in reaction $r_{i,$	dN	Detrital organic nitrogen	
fVector function of state equations (see Table A1) $k_i(T)$ Henry's law coefficient for solute $i$ Pa m³ mmol <sup>-1</sup> $k_i(T)$ Air-water gas transfer coefficient, liquid sidePa m³ d <sup>-1</sup> $k_w$ Optimization discounting parameterd <sup>-1</sup> $n_c$ Number of chemical speciesNumber of pid points for discretizing control variables over an optimization interval (see Table 18.2)Pa $n_s$ Number of biological structures, $\widehat{\gg}_j$ Pa $n_s$ Number of sub-reactions associated with $\widehat{\gg}_j$ Pa $p_i$ Partial pressure of gas species $i$ Pa $p_i^f$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t$ Optimization intervald $t$ Timed $u$ Vector of control variables ( $e, \omega$ ) $m^3 d^{-1}$ $x$ Vector of state variables ( $e, p, e_s$ ) $m^3 d^{-1}$ $F_L$ Liquid flow rate to microcosmsm³ d <sup>-1</sup> $A_r G_{r_{ij}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ kJ k <sup>-1</sup> $\widehat{\$}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ K $X$ Vector of microcosmm <sup>-3</sup> $a_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $i_j$ Oxygen atoms in unit carbon formula for biological structure $i$ $i_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $k_j$ Substate affinity parameter in reaction $r_{i,$	$f_{\rm PL}$	Fraction of particulate matter loss due to dilution	
$k_i(T)$ Henry's law coefficient for solute $i$ Pa m³ mmol <sup>-1</sup> $k_La$ Air-water gas transfer coefficient, liquid side $m^3 d^{-1}$ $k_w$ Optimization discounting parameter $d^{-1}$ $n_c$ Number of chemical species $d^{-1}$ $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n^3$ $n_S$ Number of sub-reactions associated with $\widehat{\gg}_j$ $P_a$ $p_i$ Partial pressure of gas species $i$ $Pa$ $p_i^f$ Partial pressure of gas species $i$ in feed gas $Pa$ $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization interval $d$ $\Delta t$ Utector of control variables ( $c, \omega$ ) $m^3 d^{-1}$ $\mathbf{x}$ Vector of state variables ( $c, \phi$ ) $m^3 d^{-1}$ $\mathbf{x}$ Vector of state variables ( $c, \phi$ ) $m^3 d^{-1}$ $\mathbf{x}$ Gas constant (units depend on equation) $\mathbf{x}$ $S$ System entropy $\mathbf{k}$ $\mathbf{K}^{-1}$ $\widehat{\boldsymbol{S}}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $m^{-3}$ $T$ Temperature $\mathbf{K}$ $V_G$ Gas volume of microcosm $m^{-3}$ $i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ <	f	Vector function of state equations (see Table A1)	
$k_L a$ Air-water gas transfer coefficient, liquid side $m^3 d^{-1}$ $k_w$ Optimization discounting parameter $d^{-1}$ $n_c$ Number of chemical species $d^{-1}$ $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ $n_{sj}$ Number of sub-reactions associated with $\Re_j$ $p_i$ $Pa$ $p_i$ Partial pressure of gas species $i$ $Pa$ $p_i^f$ Partial pressure of gas species $i$ in feed gas $Pa$ $p_i^f$ Reaction ratemmol $m^{-3} d^{-1}$ $\Delta t$ Optimization update interval $d$ $\Delta t$ Optimization interval $d$ $\Delta t$ Optimization interval $d$ $\Delta t$ Coptimization interval $d$ $\Delta t$ Optimization interval $m^3 d^{-1}$ $K_L$ Liquid flow rate to microcosms $m^3 d^{-1}$ $F_L$ Liquid flow rate to microcosms $m^3 d^{-1}$ $K_L$ Gas constant (units depend on equation) $S$ $S$ System entropy $KJ K^{-1}$ $\Re_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $K^-1$ $T$ Temperature $K$ $V_G$ Gas volume of microcosm $m^{-3}$ $a_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_i$ Substrate affinity parameter in reaction $r_{i,j}$ <th< td=""><td><math>k_i(T)</math></td><td>Henry's law coefficient for solute <i>i</i></td><td><math>Pa m^3 mmol^{-1}</math></td></th<>	$k_i(T)$	Henry's law coefficient for solute <i>i</i>	$Pa m^3 mmol^{-1}$
$k_w$ Optimization discounting parameter $d^{-1}$ $n_c$ Number of chemical species $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of biological structures, $\tilde{\mathfrak{S}}_j$ $n_s$ Number of sub-reactions associated with $\tilde{\mathfrak{S}}_j$ $n_s$ Number of sub-reactions associated with $\tilde{\mathfrak{S}}_j$ $Pa$ $p_i$ Partial pressure of gas species $i$ in feed gas $Pa$ $p_i^f$ Partial pressure of gas species $i$ in feed gas $Pa$ $r_{i,j}$ Reaction rate $mmol m^{-3} d^{-1}$ $\Delta t$ Optimization update interval $d$ $\Delta t$ Optimization interval $d$ $t$ Time $d$ $u$ Vector of control variables ( $\mathfrak{e}, \mathfrak{o}$ ) $\mathbf{x}$ $Y$ Vector of state variables ( $\mathfrak{e}, \mathfrak{p}, \mathfrak{e}_s$ ) $\mathbf{m}^3 d^{-1}$ $F_G$ Gas flow rate to microcosms $\mathbf{m}^3 d^{-1}$ $R$ Gas constant (units depend on equation) $S$ System entropy $\tilde{\mathfrak{S}}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $T$ $T$ Temperature $K$ $V_G$ Gas volume of microcosm $m^{-3}$ $a_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Gibus fine energy for biological structure $i$ $\beta_i$ Gibus fine energy for biological structure $i$ $\beta_i$ Gibus fine energy for biological structure $i$ $\beta_i$ Goxygen atom	$k_L a$	Air-water gas transfer coefficient, liquid side	$m^3 d^{-1}$
$n_c$ Number of chemical species $n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_s$ Number of biological structures, $\tilde{\mathfrak{S}}_j$ $n_s$ Number of sub-reactions associated with $\tilde{\mathfrak{S}}_j$ $p_i$ Partial pressure of gas species $i$ Pa $p_i^f$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t$ Optimization intervald $t$ Timed $u$ Vector of control variables ( $\mathfrak{e}, \mathfrak{w}$ ) $\mathfrak{X}$ $X$ Vector of state variables ( $\mathfrak{e}, \mathfrak{p}, \mathfrak{e}_s$ ) $\mathfrak{M}^3$ d <sup>-1</sup> $F_L$ Liquid flow rate to microcosms $\mathfrak{m}^3$ d <sup>-1</sup> $R$ Gas constant (units depend on equation) $S$ $S$ System entropy $kJ$ K <sup>-1</sup> $\tilde{\mathfrak{S}}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $\mathfrak{K}$ $T$ TemperatureK $V_G$ Gas volume of microcosm $\mathfrak{m}^{-3}$ $a_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup> $\pi^{-1}$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	$k_w$	Optimization discounting parameter	$d^{-1}$
$n_{knots}$ Number of grid points for discretizing control variables over an optimization interval (see Table 18.2) $n_{\rm S}$ Number of biological structures, $\mathfrak{S}_j$ $n_{\rm S}$ Number of sub-reactions associated with $\mathfrak{S}_j$ $p_i$ Partial pressure of gas species $i$ Pa $p_i^{f}$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t$ Optimization intervald $\Delta t^*$ Optimization intervald $\Delta t$ Stort of control variables ( $\boldsymbol{e}, \boldsymbol{\omega}$ ) $\boldsymbol{x}$ $\mathbf{v}$ cetor of control variables ( $\boldsymbol{e}, \boldsymbol{\omega}$ ) $\boldsymbol{x}$ $\mathbf{X}$ Vector of control variables ( $\boldsymbol{e}, \boldsymbol{\omega}$ ) $\mathbf{x}$ $\mathbf{X}$ Vector of state variables ( $\boldsymbol{c}, \mathbf{p}, \mathbf{e}_{\mathrm{S}}$ ) $\mathbf{M}^3 d^{-1}$ $f_L$ Liquid flow rate to microcosms $\mathbf{m}^3 d^{-1}$ $\Delta_r G_{r_{ij}}$ Gibbs free energy of reaction for reaction $r_{ij}$ $\mathbf{K}$ $\mathcal{S}$ System entropy $\mathbf{k}$ $\mathbf{K}^{-1}$ $\mathfrak{S}_j$ Biological structure $j$ that catalyzes reaction $r_{ij}$ $\mathbf{m}^{-3}$ $T$ Temperature $\mathbf{K}$ $V_G$ Gas volume of microcosm $\mathbf{m}^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Substrate affinity parameter in reaction $r_{ij}$ $\mathbf{mol}$	$n_c$	Number of chemical species	
$n_{\rm S}$ Number of biological structures, $\widehat{\Longrightarrow}_j$ $n_{\rm S_j}$ Number of sub-reactions associated with $\widehat{\Longrightarrow}_j$ $p_i$ Partial pressure of gas species $i$ in feed gasPa $p_i^f$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t^*$ Optimization intervald $t$ Timed $u$ Vector of control variables $(\varepsilon, \omega)$ $x$ $\mathbf{x}$ Vector of state variables $(\varepsilon, \mathbf{p}, \mathbf{c}_S)$ $\mathbf{m}^3 d^{-1}$ $F_L$ Liquid flow rate to microcosms $\mathbf{m}^3 d^{-1}$ $\Delta_r G_{r_{i,j}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ kJ monol <sup>-1</sup> $R$ Gas constant (units depend on equation) $S$ System entropy $S_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $K$ $V_G$ Gas volume of microcosm $\mathbf{m}^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Gow the efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$	n <sub>knots</sub>	Number of grid points for discretizing control variables over an optimization interval (see Table 18.2)	
$n_{S_i}$ Number of sub-reactions associated with $\widehat{\Rightarrow}_j$ $p_i$ Pattial pressure of gas species $i$ in feed gasPa $p_i^f$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t^*$ Optimization intervald $t$ Timed $u$ Vector of control variables $(\varepsilon, \omega)$ $x$ $\mathbf{x}$ Vector of state variables $(\varepsilon, \mathbf{p}, \mathbf{e}_S)$ $\mathbf{m}^3 d^{-1}$ $F_L$ Liquid flow rate to microcosms $\mathbf{m}^3 d^{-1}$ $\Delta_r G_{r_{i,j}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ kJ mmol <sup>-1</sup> $R$ Gas constant (units depend on equation) $S$ System entropy $S_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $\mathbf{K}$ $T$ TemperatureK $V_G$ Gas volume of microcosm $\mathbf{m}^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol $\mathbf{m}^{-3}$	n <sub>S</sub>	Number of biological structures, $\mathfrak{B}_{j}$	
$p_i$ Partial pressure of gas species $i$ in feed gasPa $p_i^f$ Partial pressure of gas species $i$ in feed gasPa $r_{i,j}$ Reaction ratemmol m <sup>-3</sup> d <sup>-1</sup> $\Delta t$ Optimization update intervald $\Delta t^*$ Optimization intervald $t$ Timed $u$ Vector of control variables $(\boldsymbol{c}, \boldsymbol{p}, \boldsymbol{c}_{S})$ $\boldsymbol{K}$ $F_G$ Gas flow rate to microcosms $\boldsymbol{m}^3 d^{-1}$ $r_L$ Liquid flow rate to microcosms $\boldsymbol{m}^3 d^{-1}$ $\Delta_r G_{r_{i,j}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ KJ K <sup>-1</sup> $\boldsymbol{S}$ System entropyKJ K <sup>-1</sup> $\boldsymbol{S}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $\boldsymbol{K}$ $V_G$ Gas volume of microcosm $\boldsymbol{m}^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\boldsymbol{\gamma}_i$ $\boldsymbol{\gamma}_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\boldsymbol{\kappa}_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol $\boldsymbol{m}^{-3}$	$n_{S_j}$	Number of sub-reactions associated with $\mathfrak{B}_i$	
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xVector of state variables (c, p, c_s) $F_G$ Gas flow rate to microcosms $m^3 d^{-1}$ $F_L$ Liquid flow rate to microcosms $m^3 d^{-1}$ $\Delta_r G_{r_{ij}}$ Gibbs free energy of reaction for reaction $r_{ij}$ kJ mmol <sup>-1</sup> RGas constant (units depend on equation) $S$ SSystem entropykJ K <sup>-1</sup> $\widehat{\mathfrak{S}}_j$ Biological structure $j$ that catalyzes reaction $r_{ij}$ $K$ TTemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol $m^{-3}$	u	Vector of control variables $(\varepsilon, \omega)$	
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$G_L$ Liquid flow rate to microcosms $m^3 d^{-1}$ $\Delta_r G_{r_{ij}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ kJ mmol <sup>-1</sup> $R$ Gas constant (units depend on equation) $K$ $S$ System entropykJ K <sup>-1</sup> $\mathfrak{S}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $K$ $T$ TemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $v_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol $m^{-3}$	FG	Gas flow rate to microcosms	$m^3 d^{-1}$
$\Delta_r G_{r_{ij}}$ Gibbs free energy of reaction for reaction $r_{i,j}$ kJ mmol^{-1} $R$ Gas constant (units depend on equation) $S$ $S$ System entropykJ K^{-1} $\widehat{\mathfrak{S}}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $K$ $T$ TemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $v_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$	$F_{I}$	Liquid flow rate to microcosms	$m^3 d^{-1}$
RGas constant (units depend on equation)SSystem entropykJ K^{-1} $\mathfrak{S}_{j}$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ $\mathcal{K}_{j}$ TTemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $V_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	$\Delta_r G_{r}$	Gibbs free energy of reaction for reaction $r_{i,i}$	kJ mmol <sup>-1</sup>
SSystem entropykJ K^{-1} $\mathfrak{B}_j$ Biological structure $j$ that catalyzes reaction $r_{i,j}$ K $T$ TemperatureK $V_G$ Gas volume of microcosmm^{-3} $V_L$ Liquid volume of microcosmm^{-3} $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure i $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m^{-3}	R	Gas constant (units depend on equation)	
$\mathfrak{S}_{j}$ Biological structure $j$ that catalyzes reaction $r_{ij}$ $T$ TemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $V_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure $i$ $\beta_i$ Oxygen atoms in unit carbon formula for biological structure $i$ $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol $m^{-3}$	S	System entropy	$kJ K^{-1}$
TTemperatureK $V_G$ Gas volume of microcosm $m^{-3}$ $V_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure i $\varepsilon_j$ Growth efficiency for biological structure j. (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m^{-3}	H <sub>i</sub>	Biological structure <i>j</i> that catalyzes reaction $r_{i,j}$	
$V_G$ Gas volume of microcosm $m^{-3}$ $V_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure i $\varepsilon_j$ Growth efficiency for biological structure j. (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	T	Temperature	К
$V_L$ Liquid volume of microcosm $m^{-3}$ $\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure i $\varepsilon_j$ Growth efficiency for biological structure j. (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	$V_G$	Gas volume of microcosm	$m^{-3}$
$\alpha_i$ Hydrogen atoms in unit carbon formula for biological structure i $\beta_i$ Oxygen atoms in unit carbon formula for biological structure i $\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure i $\varepsilon_j$ Growth efficiency for biological structure j. (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	VL	Liquid volume of microcosm	$m^{-3}$
$β_i$ Oxygen atoms in unit carbon formula for biological structure i $γ_i$ Nitrogen atoms in unit carbon formula for biological structure i $ε_j$ Growth efficiency for biological structure j. (Optimal control variable) $κ_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	$\alpha_i$	Hydrogen atoms in unit carbon formula for biological structure i	
$\gamma_i$ Nitrogen atoms in unit carbon formula for biological structure $i$ $\varepsilon_j$ Growth efficiency for biological structure $j$ . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ $mmol\ m^{-3}$	$\beta_i$	Oxygen atoms in unit carbon formula for biological structure i	
$\epsilon_j$ Growth efficiency for biological structure <i>j</i> . (Optimal control variable) $\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	γ <sub>i</sub>	Nitrogen atoms in unit carbon formula for biological structure <i>i</i>	
$\kappa_j$ Substrate affinity parameter in reaction $r_{i,j}$ mmol m <sup>-3</sup>	ε <sub>i</sub>	Growth efficiency for biological structure <i>j</i> . (Optimal control variable)	
	κ <sub>i</sub>	Substrate affinity parameter in reaction $r_{i,i}$	$\mathrm{mmol}\ \mathrm{m}^{-3}$
$v_i$ Maximum specific reaction rate for reaction $r_{i,i}$ d <sup>-1</sup>	$v_i$	Maximum specific reaction rate for reaction $r_{i,i}$	$d^{-1}$
$\sigma$ Entropy produced from irreversible processes within system kJ K <sup>-1</sup>	σ	Entropy produced from irreversible processes within system	$kJ K^{-1}$
$\dot{\sigma}$ Rate of internal entropy production kJ K <sup>-1</sup> d <sup>-1</sup>	σ	Rate of internal entropy production	$kJ K^{-1} d^{-1}$
$\chi_G$ Parameter in free energy weighting function, $f_G$ mmol kJ <sup>-1</sup>	χ <sub>G</sub>	Parameter in free energy weighting function, $f_G$	mmol kJ <sup>-1</sup>

(continued)

**Author Proof** 

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#### Table A.2 (continued)

Variable	Definition	Units
$\omega_{i,j}$	Partition coef. of biological structure j to sub-reaction $r_{i,j}$ . (Optimal control variable)	
$\Lambda_{i,j,k}$	Stoichiometric exponent for reaction $r_{ij}$ for $c_k$	
$\langle \rangle$	Expectation operator	

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